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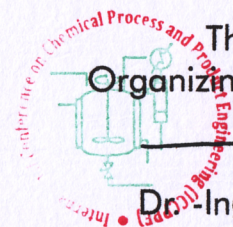
In the INTERNATIONAL CONFERENCE ON CHEMICAL PROCESS AND PRODUCT ENGINEERING 2016 (ICCPPE 2016)
Noormans Hotel, Semarang, Indonesia, September 14th-15th, 2016

On behalf of Dean of Faculty of Engineering,
Vice Dean for Academic Affairs
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Semarang, August 22nd, 2016

No. : 42/AA/ICCPPE/VIII/2016
App. : 4
Subject : **Accepted abstract ICCPPE 2016**

Dear Sir/Madam,

We are pleased to inform you that your abstract:

Title : Kinetics study the decomposition of the cellulose into cellulose nanocrystals by hydrothermal with hydrochloric acid catalyst

Author : Zul Nazri, Achmad Roesyadi, Sumarno, Fika Anjana

Code : A-3

has been accepted and will be presented for oral presentation in the International Conference on Chemical Process and Product Engineering (ICCPPE) 2016 organized by Department of Chemical Engineering Diponegoro University. The ICCPPE will be held in Noormans Hotel-Semarang on 14th -15th September 2016. Please note that this acceptance letter is also considered as **an invitation letter**.

Hence, we would like you to submit the abstract and full-paper manuscript which have been formatted according to the templates together with the CV of the presenter (please kindly find the files in the attachments). The files should be saved as **“code-abstract”, “code-paper” and “code-cv”**, respectively. Please email the files to iccppeundip@gmail.com before **10th September 2016**. The manuscript will be peer-reviewed and the selected one will be published in **Bulletin of Chemical Reaction Engineering & Catalysis** and **Advanced Science Letter**, which is indexed by Scopus.

We would like to remind you that the due date for early-bird payment is **22nd-31st August 2016**.

We are looking forward to seeing you in Semarang.

Sincerely,

Dr.-Ing. Suherman

Conference Chair, Organizing Committee

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Lampiran 4. Conference international “The International Conference on Chemical Process and Product Engineering (ICCPPE) 2016

Kinetics study the decomposition of the cellulose into cellulose nanocrystals by hydrothermal with hydrochloric acid catalyst

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Abstract: Cellulose nanocrystals hydrolyzed cellulose-based biomass residues from oil palm by using hydrochloric acid under hydrothermal conditions. ~~The characterization~~ of cellulose nanocrystals was determined by Fourier transform infrared spectroscopy and X-ray diffraction. The Infrared Spectroscopy showed there has been a removal of lignin and hemicellulose in the spectrum. Crystallinity which reaches 78.59% was obtained by hydrolysis using hydrochloric acid catalyst 3 mol/L with a reaction time of 1 hour. Based on the graph of $-\ln C_A/C_{A0}$ vs time obtained that Cellulose nanocrystals forming reaction is of first order. The reaction rate constants to the formation of glucose (k_2) is greater than the reaction rate constant to the formation of Cellulose nanocrystals (k_1), which indicates that the phase of slow reaction is the reaction of the most influential on the overall reaction rate, the reaction of the formation of Cellulose nanocrystals.

Keywords: Cellulose, CNCs, hydrothermal, hydrochloric acid

INTRODUCTION

Biomass residue oil palm is abundant and renewable biomass in nature. Biomass is also called lignocellulosic waste because the main content are cellulose, hemicellulose and lignin. Cellulose is the molecule soluble in acid but does not easily dissolve in alkali, while the hemicellulose and lignin molecules soluble in alkali but not easily soluble in acid, so the hemicellulose and lignin easily removed from cellulose by using an alkali [1].

Cellulose nanocrystals (CNCs) can be synthesized from cellulose using acid catalyst, wherein the acid initially degrades amorphous regions of cellulose chain, further fragmentation by using sonication or hydrothermally to produce nanocrystals. Some common methods that have been used to synthesize CNCs are hydrolysis using sulfuric acid, unfortunately many crystalline cellulose is degraded, so that the yield obtained less than 35% [2] and the resulting product shows a low thermal stability [3-5]. Hydrolysis of cotton pulp fibers by optimizing the preparation conditions using sulfuric acid can only increase the yield becomes 63.8% [6]. Hydrolysis of cellulose-fiber sisal using 60% H_2SO_4 can improve the crystallinity index nanocellulose to 72% and a particle size of 9.1 nm [1].

Some low concentration of mineral acids such as hydrochloric acid and maleic acid can be used to prevent aggregation and degradation of CNCs [7-10]. Rosa and Correa reported that CNCs produced by hydrochloric acid hydrolysis showed high thermal stability, but that tends to provide liquid suspension flocculation and this can only be achieved with a low yield of 20% [11-12]. Filson and Andoh utilize high power ultrasonic irradiation with short periods of sonication have produced CNCs with a crystallinity of 78%, but the yield achieved only 5% [13]. Tang et al. reported the hydrolysis method of cation-exchange resin can be applied to produce CNCs with the yield obtained 50.04% and reached 84.26% crystallinity, but the removal of the cation-exchange resin with recurrent post-treatment can be time consuming chemical and many [14].

According to Yu et al., the high yield and crystallinity is evident from the use of hydrochloric acid because the acid penetrates quickly into the deep layers of the network of cellulose and hydrolyze the amorphous regions chains of cellulose, while the crystalline regions are more resistant to acid hydrolysis lighter because the strength of hydrogen bonds between cellulose molecules adjacent compared with amorphous regions [10]. Hydrolytic reaction was also limited by the relatively short reaction time so that the acid can only degrade amorphous regions in the cellulose [10].

In this study, cellulose fibers hydrolyzed using hydrochloric acid to produce CNCs by hydrothermal processes. This process is more depth than the influence of the reaction time to the CNCs. Pursuant yield obtained CNCs do approach to the study of reaction kinetics in order to obtain the appropriate reaction order for this process.

EKSPERIMENTAL

Materials

Biomass residue oil palm was taken from crude palm oil processing plant. Chemical substance that was used for residue oil palm extraction is 17,5% wt NaOH from Merck and 2% wt NaOCl were purchased from PT. Bratachem. Acid solution that was used for cellulose hydrolysis is hydrochloric acid 3 mol/L from Merck. Aquadest that was used for washing the CNCs is taken from PT. Bratachem.

Preparation of Cellulose

50 grams of dry weight residue oil palm was included in the 17.5% wt NaOH (1:10) w/v, and then it was extracted at 80 °C for 2 hours. Extract that obtained bleaching with 250 mL of 2% wt NaOCl at 70 °C for 1 hour was also performed. Then, producted obtained was filtered and washed until neutrals.

Preparation of Cellulose Nanocrystals

Cellulose 6:360 3M HCl (g:mL) was inserted in the ultrasonics bath tipe SU-27 TH capacity 477(W) x 272(D) x 200(H) mm, frequencies 28 kHz, output 300 watts and heater 500 watts, during 30 minutes. After that, sample hydrolyzed in the hydrothermal Parr USA pressure batch reactor, then the reactor tube was closed tightly and N₂ gas was flowed into the reactor. The reaction was run at a temperature of 110 °C with a reaction time of 0; 1; 2; 3; 4 and 5 hours. After reaching the cellulosic suspension sampling time, the suspension obtained is added sufficient distilled water to stop the acid reaction, decanted in a bottle 1 to 2 days to precipitate particles of crystalline cellulose, and then washed with distilled water until neutral, centrifuged and dried.

Characterization

Fourier Transform Infrared Spectroscopy

The chemical structures of OPEFB and the resulting cellulose were characterized on a Nicolet 8700 FT-IR spectrophotometer. FT-IR spectra were recorded in the spectral range of 4000–400 cm⁻¹.

X-Ray Difrraction

The crystal structures were characterized on a Philips PZ1200 X-ray diffraction (X-RD) by using Cu K α X-rays with a voltage of 40 kV and a current of 30 mA. X-ray diffraction data were collected over an angular range of 0–50 in steps of 0,02° at room temperature. The crystallinity (CrI) of the samples was determined by Segal's method [15].

$$X_c = \frac{I(\text{crystalline}) - I(\text{amorf})}{I(\text{crystalline})} 100 \%$$

where $I_{(\text{crystalline})}$ is the intensity of the crystalline peak at the maximum at 2θ between 22 and 23 and $I_{(\text{am})}$ is the intensity at the minimum at 2θ between 18 and 19, where θ is the corresponding Bragg angle. The crystallite sizes were estimated from the 110, 110, and 200 lattice planes of cellulose I by using the well-known Scherrer equation.

$$D_{hkl} = \frac{K \cdot \lambda}{B_{hkl} \cdot \cos \theta}$$

where D_{hkl} is the crystallite size in the direction normal to the hkl family of lattice planes, K is the Scherrer constant (1.00 for equatorial reflections of rod-like or needlelike crystallites), λ is the wavelength of the radiation (1.54 Å), and B_{hkl} is the full width at half-maximum (FWHM) in radians of the reflection of that family of lattice planes [10].

RESULT AND DISCUSSION

A. Physic Analysis

Physically the change of OPEFB may be seen in Fig 1, OPEFB colors that has been treated alkali (NaOH 17,5%) becomes clearer. It showed reduced levels of lignin and hemicellulose that contained in OPEFB. Then after the hydrolysis, cellulosa nanocrystal showed whiter color.

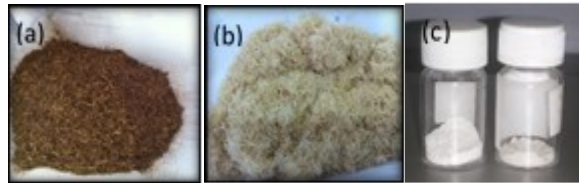


Figure 1. Physically of (a) OPEFB untreated (b) Cellulose (c) Cellulose nanocrystal

B. Condition Preparation Cellulose Nanocrystals

Table 1 shown the yield, crystallinity and crystallite size of CNCs hydrolyzed using hydrochloric acid catalyst by hydrothermal process. All parameter using the ratio of cellulose-to-acid 6 g / 360 mL with reaction temperature of 110 °C. Figure 2 shows the longer the reaction time, the yield obtained tends to be down, this is due to long reaction times hydrochloric acid can attack the cellulose crystalline regions thus reducing the crystallinity of CNCs. According to Yu et al., hydrolytic reaction is limited by the relatively short reaction time so that the acid can only be lowered amorphous regions in the cellulose and leave the crystal region. So that the reaction time is believed to be one of the most important parameters to be considered to improve the quality of CNCs [10].

TABLE I. YIELD, CRYSTALLINITY AND CRYSTALLITE SIZE OBTAINED THROUGH HYDROLYSIS USING HCl

Sample name	Process	Reaction time (hour)	Yield	X-RD	
				Crystallinity (CrI)	Crystallite size (D_{hkl})
Cellulose	extraction	-	-	61.37	29.35
CNCs-C0	hydrolysis using 3 mol/L HCl	0	0	0	0
CNCs-C1		1	74.82	78.59	7.83
CNCs-C2		2	66.00	77.07	1.81
CNCs-C3		3	46.62	76.85	3.91
CNCs-C4		4	36.41	76.62	1.81
CNCs-C5		5	28.33	73.27	4.70

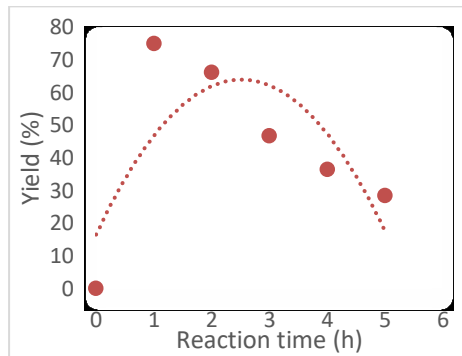


Figure 2. Graph relationship yield of CNCs vs reaction time

C. Crystallinity

Figure 3 shows the X-ray diffraction pattern of cellulose and CNCs prepared by hydrolysis of hydrochloric acid 3 mol/L. All the diffraction pattern for the cellulose crystals showed peaks around $2\theta = 16^\circ$, 22° and 35° , minimum diffraction pattern for amorphous plane showed around $2\theta = 18^\circ$ and 19° . Compared to cellulose, CNCs have broader peaks. It benefited as hydrochloric acid is more efficient in the removal of polysaccharides noncellulosic and dissolution of the amorphous zone, so CNCs have higher crystallinity [10].

Crystallinity CNCs-C1 which reaches 78.59% believed that the hydrolysis reaction using hydrochloric acid catalyst in a reaction time of 1 hour can help up to removal amorphous cellulose chains. Furthermore, the crystallinity declined slowly with increasing reaction time, as seen in the CNCs-C2 fell to 77.07% and CNCs-C5 with a longer reaction time dropped further to 73.27% This is due to the long time of the hydrolysis reaction may degrade fraction of crystalline regions of cellulose so degraded into simpler chain. Hydrochloric acid hydrolysis with reaction time is too long can weaken the cellulose crystalline regions, even resulting in carbonization CNCs [10].

CNCs shown maximum crystal diffraction peaks located at the angle $2\theta = 22.6^\circ \pm 0.2$ with 002 lattice planes, which shows crystalline cellulose I [16-17]. At an angle $2\theta = 35^\circ$ all diffraction pattern still shows a peak crystalline cellulose are low, this indicates that hydrochloric acid catalyst capable of persevering region crystals that are at the peak of the weak areas [16]. Overall CNCs shows the crystallite size below 7.83 nm, this proves that the hydrolysis using acid catalysts are applied can reduce the size of crystalline cellulose.

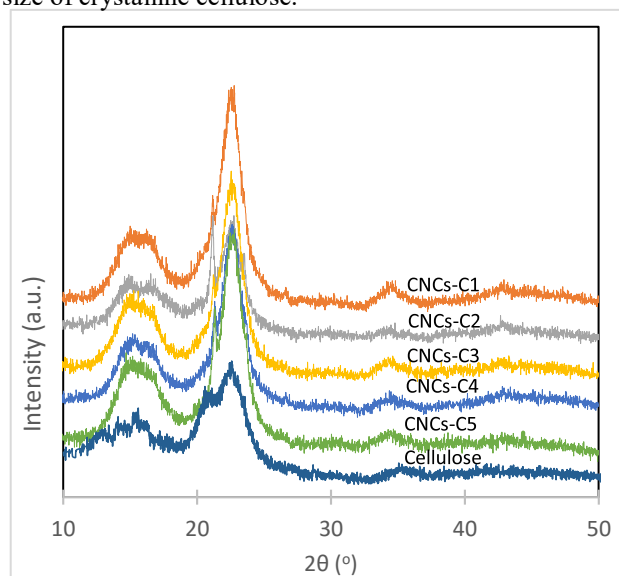


Figure 3. XRD of cellulose and CNCs are hydrolyzed with a reaction time of 1 to 5 hours

D. Chemical Structure

The FT-IR spectrum in Figure 4 shown all the CNCs displaying a broad absorption peaks located at 3250-3500 cm^{-1} which is a stretch -OH group. The absorption peak at 2890-2920 cm^{-1} region associated with the group -CH₂, while at the peak absorption 2890 and 2900 cm^{-1} is an overlapping of tape -CH², this peak is only found in cellulosic feedstocks, while at the peak CNCs have been lost due to the amorphous cellulose chain termination.

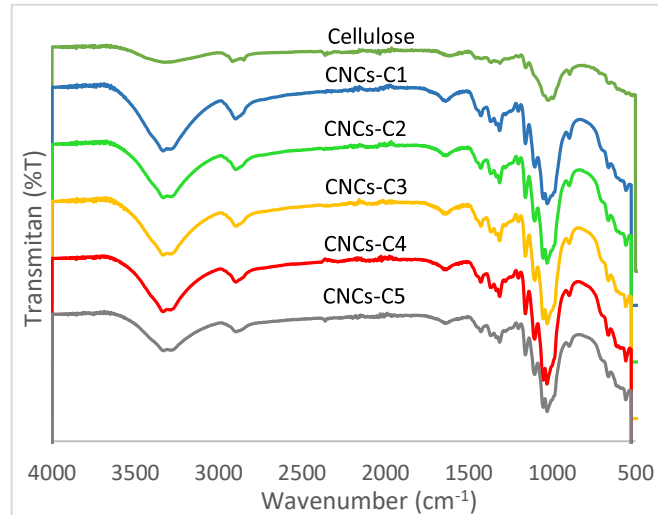


Figure 4. The FT-IR spectrum cellulose and CNCs are hydrolyzed with a reaction time of 1 to 5 hours

Absorption in the 1600-1650 cm^{-1} in the samples cellulose is an indication of the absorption of water or stretch O-H, in the spectrum absorption peaks are already getting smaller this is because the crystal structure is already happening removal of water. According to Johar et al., this peak indicates the bending form water molecules due to a strong interaction between cellulose and water [18]. Absorption peaks in the region 1300-1365 cm^{-1} in all samples a ribbon of vibration of C-H and C-O associated with aromatic rings polysaccharides [16], this absorption band according to data analyzed by the Nacos [19]. That looks sharp absorption peaks at 1000-1160 cm^{-1} caused by the deformation of vibration of C-H. According to Kagarzadeh et al., peak is a vibration deformations C-H and pyranose C-O-C is more prevalent [20]. Spectrum CNCs also shows the intensity has increased at the peak, it implies an increase in the value of crystalline cellulose [12].

E. Kinetics of reaction

Reaction series of hydrolysis of cellulose to CNCs and glucose is shown in Figure 5.

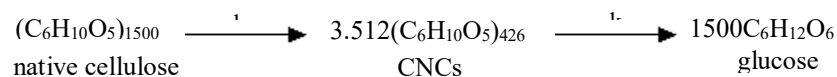


Figure 5. Reaction cellulose hydrolysis using hydrochloric acid catalyst

The above reaction can be written as:



From the reactions known initial weight was 6 g cellulose, cellulose BM is 243,000 g/mol, BM CNCs is 69,000 g/mol and BM glucose was 180.18 g/mol. As a reactant converted into product R is the yield CNCs and as product S is the concentration of glucose. Based on cellulose hydrolysis reaction is obtained kinetic model of the reaction.

The assumption of a homogeneous solution, the particles are small enough so that the resistance resulting from mass transfer can be ignored. Equation reaction speed of the reaction series, irreversible reaction is as follows:

$$r_A = \frac{dC_A}{dt} = -k_1 C_A \quad (4.1)$$

$$r_R = \frac{dC_R}{dt} = k_1 C_A - k_2 C_R \quad (4.2)$$

$$r_S = \frac{dC_S}{dt} = k_2 C_R \quad (4.3)$$

To determine the value of k_1 using the following equation:

$$-\ln \frac{C_A}{C_{A0}} = k_1 t \text{ atau } C_A = C_{A0} e^{-k_1 t} \quad (4.4)$$

$$\text{where: } C_A = C_{A0} - C_{A0} X$$

To determine the change in concentration on R, substitution of concentration A of equation (4.4) into the differential equation in the reaction speed changes for R from equation (4.2)

$$\frac{dC_R}{dt} + k_2 C_R = k_1 C_{A0} e^{-k_1 t} \quad (4.5)$$

For first-order differential equation is as follows:

$$\frac{dy}{dx} + Py = Q \quad (4.6)$$

Multiplied by a factor of integration of $e^{\int P dx}$ so be:

$$y e^{\int P dx} = \int Q e^{\int P dx} dx + \text{constant} \quad (4.7)$$

From equation (4.5) it can be seen that the integration factor $e^{k_2 t}$, while the constant of integration, namely $-\frac{k_1 C_{A0}}{(k_2 - k_1)}$, from the initial conditions $C_{R0} = 0$ to $t = 0$. So we get the final equation for the change in concentration of R is:

$$C_R = C_{A0} k_1 \left(\frac{e^{-k_1 t}}{k_2 - k_1} + \frac{e^{-k_2 t}}{k_1 - k_2} \right) \quad (4.8)$$

Stoichiometry for the concentration of reactants:

$$C_{A0} = C_A + C_R + C_S \quad (4.9)$$

From equation (4.4) and equation (4.8) is obtained:

$$C_S = C_{A0} \left(1 + \frac{k_2}{k_1 - k_2} e^{-k_1 t} + \frac{k_1}{k_2 - k_1} e^{-k_2 t} \right) \quad (4.10)$$

If k_2 is much greater than k_1 , equation (4:10) into:

$$C_S = C_{A0} (1 - e^{-k_1 t}), \quad k_2 \gg k_1 \quad (4.11)$$

The maximum concentration of R can be calculated using the equation:

$$\frac{C_{R \max}}{C_{A0}} = \left(\frac{k_1}{k_2} \right)^{k_2 / (k_2 - k_1)} \quad (4.12)$$

Based on the above equation can be determined the value of C_S , C_R , C_A and $-\ln C_A / C_{A0}$ as shown in Table 2.

TABLE II. VALUES C_S , C_R AND C_A OBTAINED FROM THE CALCULATION

Time (h)	C_{A0}	C_S	C_R	C_R+C_S	$C_{A0}X = (C_R+C_S)'$	$C_A = C_{A0} - C_{A0}X$	$-\ln C_A/C_{A0}$
0	0.0000247	0.0000000	0.0000000	0.0000000	0.0000000	0.0000247	0.0000000
1	0.0000247	0.0000012	0.0000049	0.0000061	0.0000017	0.0000230	0.0724715
2	0.0000247	0.0000024	0.0000040	0.0000064	0.0000018	0.0000229	0.0770538
3	0.0000247	0.0000044	0.0000028	0.0000072	0.0000021	0.0000226	0.0870748
4	0.0000247	0.0000073	0.0000022	0.0000095	0.0000027	0.0000220	0.1159935
5	0.0000247	0.0000105	0.0000015	0.0000119	0.0000034	0.0000213	0.1480321

From table 2 was obtained plot a graph of residual cellulose concentration (C_A) vs time, the concentration of CNCs (C_R) vs time and glucose concentration (C_S) vs time.

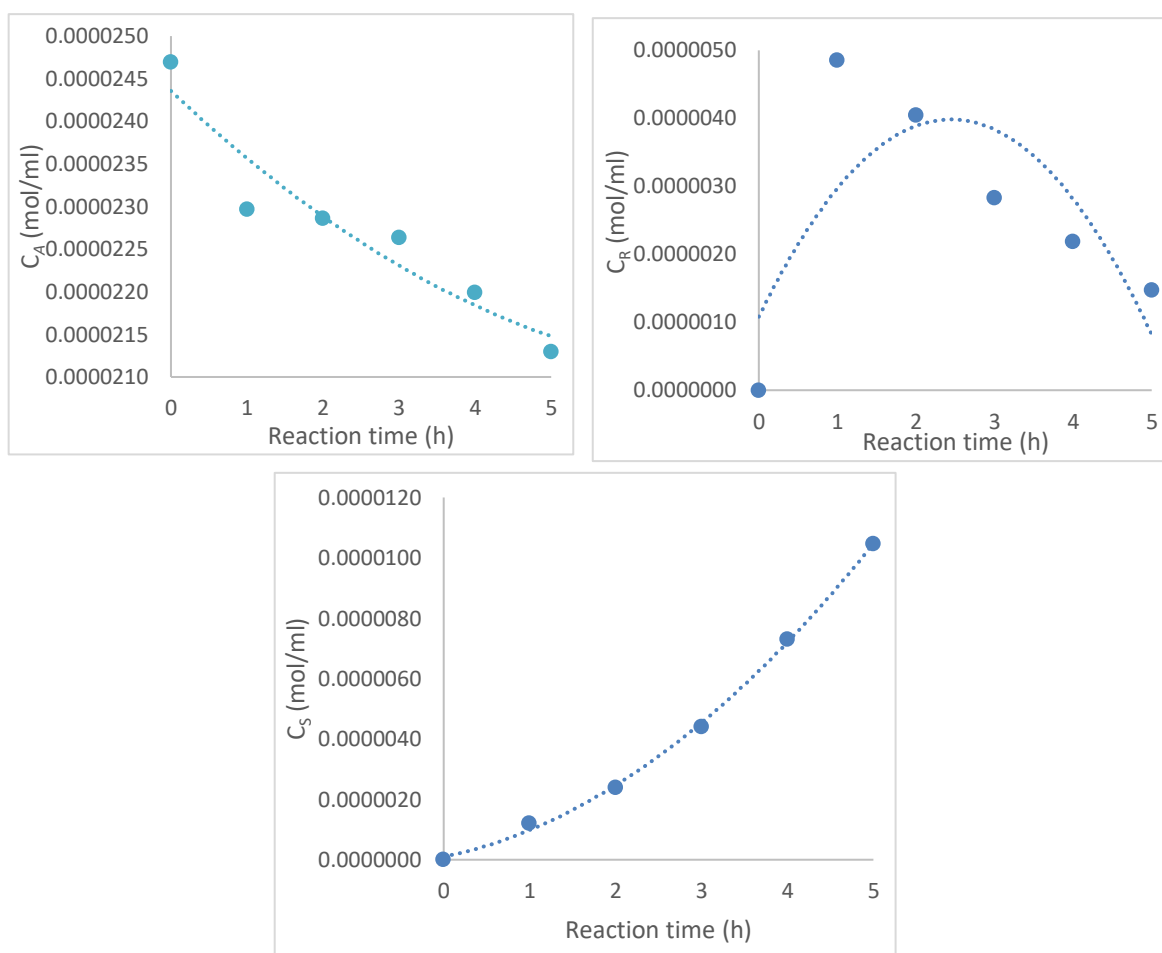


Figure 6. Relationship between (a) the concentration of residual cellulose (C_A) vs time, (b) the concentration of CNCs (C_R) vs time and (c) the concentration of glucose (C_S) vs time.

Figure 6 shows the concentration of cellulose (C_A) is reduced during the reaction, and the concentration of CNCs (C_R) increases until it reaches a peak on reaction time 1 hour, then decreased in line with the length of time the reaction is followed by increased concentrations of glucose (C_S) along the length of reaction time, so that the reaction is considered to be a series reaction. Decreased in concentration CNCs (C_R) due to excessive degradation of crystalline cellulose so that increased concentrations of glucose (C_S), so that the reaction time becomes the main influential factor in the study of the kinetics of hydrolysis of cellulose into CNCs. The graph above may not be combined

because of differences in scale. From Figure 6 obtained constant reaction (k_1) forming CNCs, by plotting this graph shows that the CNCs forming reaction is first order one.

Values k_1 and k_2 at a concentration of 3 mol/L and a temperature of 110 °C can be seen in Table 3 where the value k_2 obtained from the substitution value C_{Rmax} into the equation (4.12). C_{Rmax} is a maximum point in Figure 6(b).

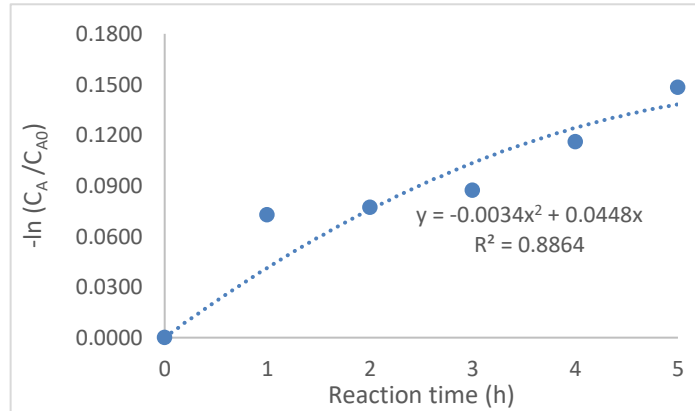


Figure 7. Relationship between $-\ln C_A/C_{A0}$ vs time

Figure 7 is a graph of $-\ln C_A/C_{A0}$ vs time obtained from the calculation of the concentration of the remainder of the initial concentrations based on data from Table 2. This graph strengthens the evidence that the longer the reaction time, the remaining reactants concentration is getting smaller, where $-\ln C_A/C_{A0}$ obtained increasing together with the increasing reaction time, so this graph reflects the equation of order 1.

TABLE III. CONSTANTS REACTION FOR 3 MOL/L HCL CATALYST

Temperature (°C)	Catalyst HCl (mol/L)	k_1 (Jam ⁻¹)	k_2 (Jam ⁻¹)
110	3	0,0308	3,545

Can be seen in Table 3, the reaction rate constant in the formation of glucose (k_2) is greater than the reaction rate constant to the formation of CNCs (k_1). This is consistent with the study of Wang et al., who reported that the constant formation reaction of glucose faster than CNCs [22]. Value $k_2 > k_1$ indicates that the slowest reaction stage is the stage of reaction greatest influence on the overall rate of reaction is the reaction of the cellulose into CNCs.

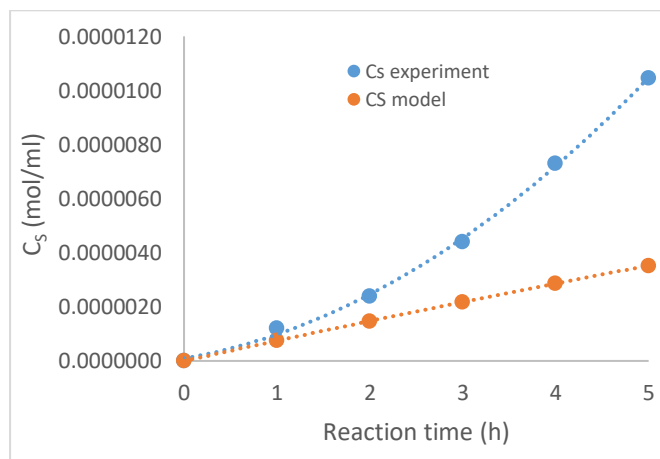


Figure 8. Relationship between glucose concentration (C_s) vs time

Figure 8 can be seen experimental glucose concentration (C_S experiment) higher than the concentration of glucose models (C_S model), it indicates that the formation of glucose can occur directly from the decomposition of the cellulose without via formation of CNCs.

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